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# A novel NiFe@NC-functionalized N-doped carbon microtubule network derived from biomass as a highly efficient 3D free-standing cathode for Li-CO<sub>2</sub> batteries



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#### ABSTRACT

Rechargeable Li-CO<sub>2</sub> batteries, which utilize CO<sub>2</sub> into electrochemical energy storage systems, provide a promising strategy for alleviating the greenhouse effect and developing high energy density second batteries. However, problems such as poor battery performance and short cycle life still hinder the development of Li-CO<sub>2</sub> batteries. In this work, a novel three-dimensional free-standing NiFe@NC/PPC cathode is prepared by depositing NiFe-Prussian blue analogues on the surface of pomelo peels (PP) and subsequently calcining at high temperature. The products fully retained the three dimensional porous characteristic of biomass, conducing to mass transfer and diffusion. In addition, the high catalytic activity of NiFe@NC is carried forward. Combined with these two advantages, the Li-CO<sub>2</sub> battery with NiFe@NC/PPC cathode exhibits a superior discharge capacity of  $6.8 \text{ mA} \text{ h cm}^{-2}$  and can sustain 109 cycles with a cutoff capacity of  $0.25 \text{ mA} \text{ h cm}^{-2}$  at a current density of  $0.05 \text{ mA} \text{ cm}^{-2}$ . Overall, this study provides a promising way for the fabrication of environmentally friendly and inexpensive cathodes to improve the performance of Li-CO<sub>2</sub> batteries.

#### 1. Introduction

Carbon dioxide ( $CO_2$ ) is the main component of the greenhouse gases, which is the culprit leading to global warming. Various methods, such as geological sequestration [1], chemical absorption [2] and so on, have been used to reduce  $CO_2$  emissions. However, these methods are of high energy consumption. Li- $CO_2$  battery is a new type of electrochemical energy storage system fueled by  $CO_2$ , which provides a feasible research idea for the reduction of  $CO_2$  emissions [3,4]. However, in fact, low specific energy density and poor cycle stability are the stumbling blocks for developing high performance Li- $CO_2$  batteries [5–7].

In order to improve the performance of  $\text{Li-CO}_2$  batteries, many efforts have been devoted to develop high active catalysts for  $\text{Li}_2\text{CO}_3$  decomposition. Zhou et al. [8] used Ru@Super P as the cathode for Li-

 ${\rm CO}_2$  batteries. They proposed that Ru nanoparticles are able to promote the reaction between  ${\rm Li}_2{\rm CO}_3$  and carbon instead of the self-decomposition of  ${\rm Li}_2{\rm CO}_3$  and thereby lower the charge potential and avoid electrolyte decomposition. The resulted cell delivered a discharge capacity as high as 8229 mA h g $^{-1}$  and showed a coulombic efficiency of 86.2% in the first discharge-recharge cycle. However, Ru is expensive and resource scarce, which is not conducive to commercialization of  ${\rm Li}_2{\rm CO}_2$  batteries. Zhou et al. [9] prepared  ${\rm Cu/N}_2$ -doped graphene through a gel-like film synthesis mechanism as the cathode catalyst for  ${\rm Li}_2{\rm CO}_2$  batteries. The addition of Cu nanoparticles improves the catalytic activity and promotes the reaction between  ${\rm Li}_2{\rm CO}_3$  and carbon during charging, resulting a low overpotential of 0.77 V and a good cyclability (50 cycles). Furthermore, they explored Ni nanoparticles/N-doped graphene composite for the cathode of  ${\rm Li}_2{\rm CO}_2$  batteries [10]. It is found that the interaction between  ${\rm Li}_2{\rm CO}_2$  and Ni is very strong based on first

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principles, suggesting that the Ni surface can effectively adsorb Li and CO $_2$ ; the Ni nanoparticles were served as the active centers for CO $_2$  reduction and evolution reactions. Most importantly, they investigated the reasons why the Li-CO $_2$  batteries with the transmission metal catalysts exhibited an excellent reversibility. During the discharge/charge cycle test, the surfaces of transmission metal nanoparticles gradually formed a thin oxide film, which can protect the cathodes from the damage caused by the self-decomposition of Li $_2$ CO $_3$ . Geng et al. prepared, via pyrolysis of ZIF-8, Co single-atom catalysts with four-coordinated N. The Co1-N4 active center promoted the binding strength between CO $_2$  and the catalysts, as well as facilitating CO $_2$  activation [11]. Pan et al. investigated the CO $_2$  reduction reaction activities of M-N-C with five transition metals and they established that Fe and Ni are more active than Co $_2$  Mn, and Cr for the reduction of CO $_2$  to CO [12].

Except metal catalysts, N-doped carbon materials were proved to have good catalytic performance for  $\mathrm{CO}_2$  reduction [13–15]. Dai et al. demonstrated that heteroatom B, N-codoped holey graphene could enhance the catalytic activity for  $\mathrm{CO}_2$  reduction and evolution reactions [16]. The resulting Li-CO $_2$  battery with B, N-codoped holey graphene displayed an excellent rate performance, outstanding reversibility, and superb long-term cycling stability, compared with that of primary holey graphene.

In this work, we prepared a composite of NiFe@NC core-shell nanoparticles highly dispersed on the free-standing N-doped carbon microtubule network, which derived from the NiFe-Prussian blue analogues/pomelo peel composite. The resulting NiFe@NC/PPC cathodes endowed Li-CO $_2$  batteries with low overpotentials, excellent cyclability, and high coulombic efficiency.

#### 2. Experimental section

### 2.1. Materials preparation

All the employed reagents were of analytical grade without further purification. Fresh pomelos were bought from the supermarket. Before being used, the pomelo skins were peeled-off and left the white inner core, and then washed with deionized water to remove impurities. The pomelo peels were cutted into small wafers with diameter of  $16~\mathrm{mm}$  and thickness of  $1-2~\mathrm{mm}$ .

NiFe-Prussian blue analogues/pomelo peel (NiFe-PBA/PP) precursors were synthesized through a coprecipitation approach according to international literature [17-19]. More specifically, 0.87 g of Ni (NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and 1.325 g of Na<sub>3</sub>C<sub>6</sub>H<sub>5</sub>O<sub>7</sub>·2H<sub>2</sub>O were dissolved in deionized water (20 mL) and then added several pieces of pomelo peels to form the solution A. Continuous magnetic stirring and ultrasonication for 2 h to ensure that pomelo peel is fully saturated with the solution. Then 0.6585 g of K<sub>3</sub>[Fe(CN)<sub>6</sub>] was dissolved in 20 mL of distilled water to form the solution B, which was slowly added into the solution A at room temperature. After the mixture was stirred for 15 min, the obtained mixed solution was aged for 24 h at room temperature. The pomelo peels covered with earth-yellow precipitations were removed, washed with deionized water and ethanol, and then dried under vacuum at 60 °C for 12 h. The as obtained PBA/PP precursors were pyrolyzed at 1000 °C in Ar atmosphere to obtain the final air-electrodes, denoted as NiFe@NC/PPC. The average mass of all NiFe@NC/PPC cathodes was 8-15 mg.

For comparison, a powder of NiFe@NC was prepared by the same process without pomelo peels. The free standing cathodes derived from pomelo peels were pyrolyzed at same temperature, named as PPC (carbonized pomelo peels). The average mass of all PPC cathodes was 5–10 mg.

#### 2.2. Material characterization

The structure of the cathodes was characterized by X-ray diff ;raction (XRD, Bruker D8 Advance) under Cu  $K_{\alpha}$  radiation. The morphology

and microstructure of the as-prepared samples were recorded using a (Hitachi SU8200 and SU8010) field-emission scanning electron microscope (SEM) and a (FEI Tecnai-20) transmission electron microscope (TEM). X-ray photoelectron spectroscopy (XPS) analysis was carried out by using a (ESCALAB 250Xi) spectroscope with Al  $\rm K_{\alpha}$  radiation to characterize the chemical compositions. All binding energy values were corrected using the internal standard of the C 1 s peak (284.8 eV) as a reference. The NiFe load content was obtained by simultaneous thermal analysis (TG/DSC, NETZSCH, TAQ600) from ambient to 800  $^{\circ}\rm C$  under flowing air.

#### 2.3. Electrochemical tests

A CR2025-type coin cell was used to perform the electrochemical tests. The cells were assembled in a glove box filled with Ar (MBRAUN,  $H_2O < 0.5$  ppm,  $O_2 < 0.5$  ppm). Cell pans were machine drilled with  $7x\Phi1.0$  mm holes in an evenly distributed pattern for  $CO_2$  access. The free-standing PPC or NiFe@NC/PPC cathodes were served as the cathode directly, while fresh Li foil was used as the anode, glass filter (Whatman grade GF/D) was employed as a separator and 1 M LiCF<sub>3</sub>SO<sub>3</sub> in tetra-ethylene glycol dimethyl ether (TEGDME) solution was used as the electrolyte. For the NiFe@NC/carbon paper (NiFe@NC/CP) and Super P/carbon paper (Super P/CP) cathodes preparation, the Super P carbon powder (Temical) or NiFe@NC catalysts mixed with polyvinylidene fluoride (PVDF) at a mass ratio of 9:1 in N-methyl-2-pyrrolidone (NMP) to form a slurry, then uniformly sprayed on carbon paper (12 mm in diameter; mass loading of  $0.8-1.0\,\mathrm{mg~cm^{-2}}$ ) and dried at 80 °C overnight in a vacuum oven. All the assembled Li-CO2 cells were transferred to a sealed glass bottle filled with 1.0 atm pure CO2 flowing for the electrochemical tests. The cell performances were evaluated by using a battery testing system (Neware, CT-3008, China) between 2.0 and 4.5 V (vs. Li<sup>+</sup>/Li) at room temperature. Before each test, the cells were rested for 5 h in CO2 atmosphere. All specific capacities of the cathodes were normalized by the total weight of the cathode.

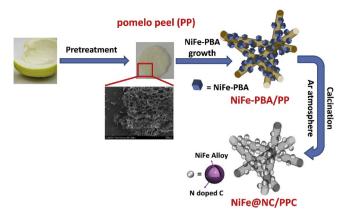
Electrochemical impedance spectroscopy (EIS) and cyclic voltammetry (CV) were performed using a PARSTAT 4000 electrochemical workstation (Princeton, USA) equipped with a frequency response analysis (FRA) module. A signal amplitude of 5 mV in the frequency range of 100 kHz to 10 mHz was applied. The anode was used as the reference and also as the counter electrode, while the cathode was used as the working electrode. The cell impedance would be mainly dominated by the cathodic impedance. Cyclic voltammetry (CV) experiments were conducted at a scan rate of 0.1 mV s $^{-1}$  between 2.0 and 4.5 V vs. Li $^+$ /Li. Cyclic tests were controlled with a cutoff capacity of 0.25 mAh cm $^{-2}$  at a current density of 0.05 mA cm $^{-2}$ .

#### 3. Results and discussion

The synthesis process of the NiFe@NC/PPC cathodes is illustrated in Scheme 1.

Firstly, a large amount of Ni<sup>2+</sup> ions were absorbed on the surface of the hydrophilic pomelo peels. After adding Fe<sup>3+</sup>, NiFe-PBA cubes were formed and the color of solution changed from green to bright yellow, and then turned to brown. Finally, the white pomelo peels became brown (Fig. S1). After high temperature calcination, the pomelo peels were carbonized and a porous carbon fiber skeleton was obtained. At the same time, NiFe ions were reduced by carbon [20,21], while the PBA cubes transformed into NiFe@NC nanoparticles with core-shell structures. The finally products were black circles (see Fig. S1), which can be directly used as the cathodes of Li-CO<sub>2</sub> batteries.

Scanning electron microscope (SEM) was employed to characterize the morphology of the NiFe-PBA/PP precursor and the produced NiFe@ NC/PPC. As can be seen in Figs. 1a–1c , the NiFe-PBA/PP precursor exhibits a porous structure under a large angle of view, which is composed of plicated microfibers. In detail, the NiFe-PBA with typical cubic shape [22], which evenly dispersed on the surface of the pomelo peel



 $\begin{tabular}{ll} Scheme 1. A schematic of the preparation procedure of NiFe@NC/PPC cathodes. \end{tabular}$ 

microfibers. The average size of these NiFe-PBA cubes is approximately 70 nm. It should be noted that NiFe-PBA cubes present a chapped surface, which is mainly caused by spraying gold before SEM testing. As shown in Figs. 1d–1f, the overall morphology of the electrode still maintains the porous structure after calcination, while the pomelo peel turn into carbon microtubules. However, things changed absolutely for NiFe-PBA cubes. The final nanoparticles present an obvious core-shell structure similar to that of frog eggs. We suggest that the relatively open large pore structure formed by interwoven carbon microtubules is beneficial to the diffusion of oxygen and electrolyte, while the micropores formed by the accumulation of NiFe@NC particles contribute to

the increase of the three-phase reaction interface. In addition, the carbon layer may be helpful to inhibit the growth and agglomeration of NiFe catalyst in the cell cycle.

The detailed architecture of NiFe@NC/PPC was observed by TEM and it is given in Fig. 2. It is clear to see that the high-resolution TEM image presents the core-shell characteristics of NiFe@NC in Fig. 2a and the calculated interplanar spacing in Fig. 2b is 0.204 nm. The corresponding EDS elemental mapping (Fig. 2c) demonstrates that C, N, Ni and Fe elements are homogeneously distributed throughout the NiFe@NC/PPC electrode. Information for the composition and structure of the as-prepared samples was obtained by X-ray diffraction (XRD). As shown in Fig. S2a, the main diffraction peaks of the Ni-Fe PBA precursor are consistent with the standard patterns of KNiFe(CN)<sub>6</sub> (JCPDS: 51-1897), without other miscellaneous peaks, illustrating that the formation of KNiFe(CN)<sub>6</sub> is without impurities [22]. In addition, the XRD pattern reveals a broad peak at around  $2\theta = 26^{\circ}$  and a less intense peak at  $43^{\circ}$  (see Fig. S2b), which matches with the (002) and (101) plane of graphitic C for pomelo peel derived carbon (PPC).

After calcining at 1000 °C, the characteristic peaks of Ni-Fe PBA precursor completely disappear, instead of the diffraction peaks of NiFe alloy (Fig. 3). The peaks at 44.3°, 51.5°, and 75.8° correspond to the (111), (200), and (220) planes of Awaruite phase FeNi<sub>3</sub> (JCPDS: 38-0419) respectively, while the characteristic carbon peak at around 26° can be indexed to (002) graphitic plane, deriving from the carbonization of -CN groups in the PBA precursor. Hence, we suggest that Ni-Fe PBA can be successfully converted into NiFe@NC after carbonization treatment. The NiFe@NC/PPC shows both the NiFe@NC and graphite related peaks, which identify the growth of Ni-Fe PBA over pomelo peel. However, the diffraction peaks of NiFe alloy in the composites of

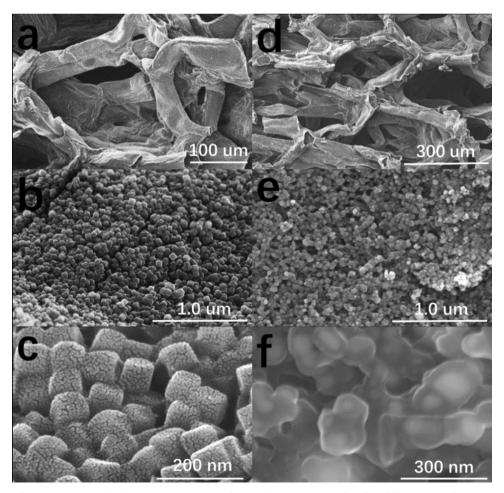
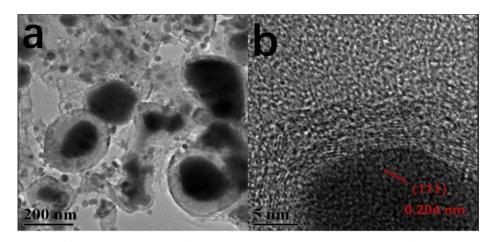


Fig. 1. SEM images of NiFe-PBA/PP precursor (a, b, c) and NiFe@NC/PPC (d, e, f) at different magnifications.



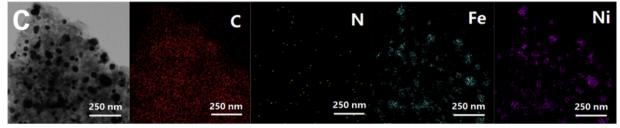


Fig. 2. TEM images of NiFe@NC/PPC (a, b) and EDS mapping of NiFe@NC/PPC (c).

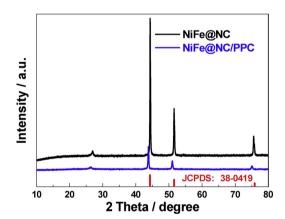


Fig. 3. XRD patterns of NiFe@NC and NiFe@NC/PPC.

NiFe@NC/PPC slightly shift left, implying that there may be a strong interaction between NiFe@NC and PPC, which would promote the  ${\rm CO_2}$  reduction electrocatalytic activity.

XPS was performed to study the composition and the corresponding chemical valence states of as-prepared samples. The entire XPS spectrum is initially corrected by the high-resolution C 1 s spectrum. From the survey scan spectrum (see Fig. S3), evident peaks for C, N, Ni and Fe are presented. As shown in Fig. 4a, the high-resolution C 1s XPS spectrum of the fresh NiFe@NC/PPC cathode could be deconvoluted into four peaks at 284.8 eV, 285.2 eV, which can be indexed to carbon in the forms of  $sp^2$  C- $sp^2$  C and N =  $sp^2$  C, respectively [23-27]. In addition, the high-resolution N 1s spectrum (Fig. 4b) reveals three components located at 398.0 eV, 399.5 eV and 400.2 eV, corresponding to pyridinic-N, metal-N and pyrrolic-N atom [28,29], respectively. This result demonstrates that the N elements in pomelo peels and the -CN groups in PBA were successfully doped into the carbon skeleton after carbonization, which may be conducive to both the CO2-reduction reaction (CO<sub>2</sub>RR) and evolution reaction (CO<sub>2</sub>ER) [16]. As seen in Fig. 4c, it is clear that the binding energy peaks at 870.3 eV and 853.5 eV correspond to Ni° [30–32]. The high-resolution Fe 2p spectrum (Fig. 4d) shows peaks centered at 707.7 eV and 720.7 eV, which can be indexed to Fe $^\circ$  2p<sub>3/2</sub> [33,34]. Whereas, peaks centered at 725.2 eV assigned to Fe 2p1/2 of Fe(III) and Fe(II),  $\approx$ 711 eV to  $\approx$ 713 eV assigned to Fe 2p3/2 of Fe(II) and Fe(III) ions, attributing to the surface oxidation of NiFe@ NC nanoparticles.

*In-situ* cyclic voltammetry (CV) was used to examine the  $CO_2$  catalytic activities of various cathodes in Li- $CO_2$  batteries from 2 to 4.5 V, as shown in Fig. 5a.

The current density (mA g $^{-1}$ ) was normalized to the weight of whole cathode. As disclosed in the cyclic voltammetry (CV) curves, the NiFe@NC/PPC cathode exhibits onset potential of 2.88 V and 3.1 V for positive and negative scan, respectively. The NiFe@NC/CP and NiFe@NC/PPC cathodes almost have similar shape, but the cathodic and anodic peaks for NiFe@NC/PPC cathodes are more obvious and the cathodic current of NiFe@NC/PPC cathodes is much higher.

These results reveal the excellent bi-functional catalytic activity of NiFe@NC/PPC for  $CO_2$  reduction reaction and  $Li_2CO_3$  decomposition. From Fig. 5b and Table S1, it is clear that the  $R_{ct}$  of NiFe@NC/PPC is smaller than that of other cathodes, indicating the fast charge transfer process with the combination of NiFe@NC catalyst and PPC support.

The galvanostatic discharge/charge performances of Li-CO $_2$  batteries with different cathodes were studied at a current density of 0.05 mA cm $^{-2}$ .

As shown in Fig. 6a, the battery with NiFe@NC/PPC cathode shows a stable discharge plateau of  $\sim 2.76\,\mathrm{V}$  with the corresponding overpotential of ca.  $0.04\,\mathrm{V}$  [35], while the discharge capacity reaches  $6.8\,\mathrm{mA}\,\mathrm{h}$  cm<sup>-2</sup>. The specific capacities of the cathodes is high up to  $518\,\mathrm{mA}\,\mathrm{h}$  mg<sup>-1</sup><sub>cathode</sub>, normalized by the total weight of cathode. More importantly, NiFe@NC/PPC shows a charge capacity of  $4.9\,\mathrm{mA}\,\mathrm{h}$  cm<sup>-2</sup> with a perfect columbic efficiency of 72.0%. These results can be favorably compared with the already published ones [5,9,10,36] (see Table 1). As can be distinguished in Fig. 6a, there is a small peak in the charging curve, which also has been reported in other literature reports [35,36]. Although in the literature there is no explanation for this phenomenon, we can speculate as follows: during the discharge process, the non-conductive and insoluble Li<sub>2</sub>CO<sub>3</sub> gradually cover the surface of catalysts forming a thick layer (see below Figs. 7a and 7b).

So, we suggest that the most intimate layer of Li<sub>2</sub>CO<sub>3</sub>, tightly coated

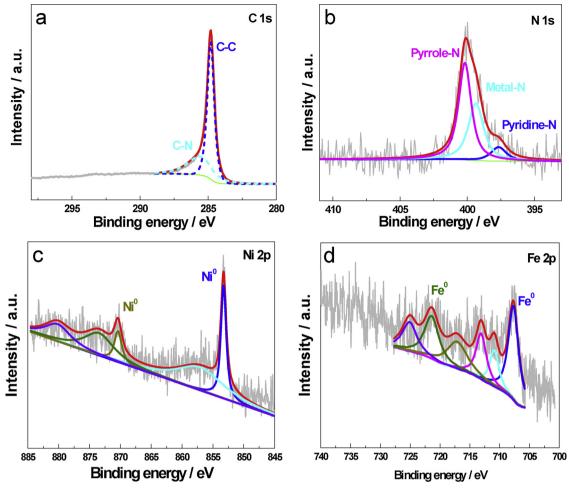


Fig. 4. XPS spectrum of NiFe@NC/PPC.

on the catalysts, is infinitely close to the three phase reaction interface. At the initial stage of charging, the most intimate layer of  $\rm Li_2CO_3$  is easily to be decomposed (voltage < 4.0 V). However, with the continuation of the charging process, a gap formed between catalysts and  $\rm Li_2CO_3$ , and these  $\rm Li_2CO_3$  away from the catalyst is hardly to receive electrons. Hence, a greater voltage (> 4.0 V) is needed to decompose the rest  $\rm Li_2CO_3$ , similar to breaking the barrier.

In contrast, the electrochemical performance related Super P/CP, NiFe@NC/CP, and individual PPC cathodes were also given. Obviously,

the cells with Super P/CP or PPC cathodes show a negligible capacity. Whereas, for NiFe@NC/CP, the electrodes were prepared by coating the slurry of NiFe@NC powder and binder on the carbon paper, resulting a specific capacity as low as  $0.4\,\mathrm{mA}\,\mathrm{h}~\mathrm{cm}^{-2}$  and a much higher overpotential compared with that of NiFe@NC/PPC.

In the previous literature [37], it can be found that the pores are mainly distributed in microporous range for catalyst coating method due to the accumulation of catalyst particles, which may cause the  $\rm CO_2$  gas and electrolyte transport channel blocking. Furthermore, the

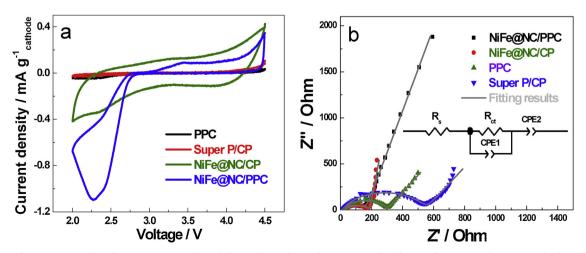


Fig. 5. In-suit cyclic voltammetry curves (a) and electrochemical impedance spectra (b) of Li-CO2 batteries with various cathodes.

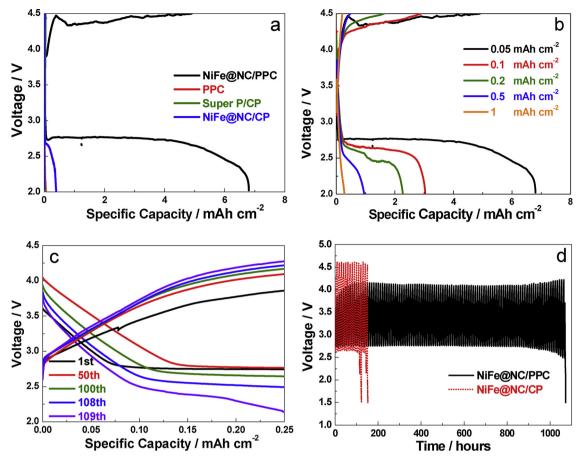


Fig. 6. (a) Charge-discharge curves of Li-CO<sub>2</sub> batteries with various cathodes. (b) Rate capability of NiFe@NC/PPC cathode at different current densities. (c) Cycling stability of NiFe@NC/PPC cathode at  $0.05 \, \text{mA} \, \text{cm}^{-2}$  with a limited capacity of  $0.25 \, \text{mAh} \, \text{cm}^{-2}$ . (d) The variation of the terminal charge and discharge voltages of NiFe@NC/PPC cathode at  $0.05 \, \text{mA} \, \text{cm}^{-2}$ .

generation of insoluble discharged products (Li<sub>2</sub>CO<sub>3</sub>) will cover on the electrode surface, which further lead to the decrease of the three-phase reaction interfaces [38]. We suggest these are the main reasons for the rapid attenuation in Li-CO<sub>2</sub> battery performance. For PPC cathode, the performance of electrocatalytic CO<sub>2</sub> reduction is poor over N-doped carbon materials, which is consistent with the CV results, leading to a poor cell performance. These results indicate that NiFe@NC/PPC cathodes possess superior electrochemical performances in Li-CO<sub>2</sub> batteries, which might be derived from the synergy of the following advantageous factors: the hybrid materials not only inherit the 3D free-standing structure of PPC and high porosity, but also exhibit high catalytic activity for CO<sub>2</sub> reduction. The plentiful and large channels of NiFe@NC/PPC provide enough volume for the deposition of discharge products, resulting in a more stable electrochemical reaction and an enhanced discharge capacity.

In Fig. 6b, the rate capability is also tested in the voltage window between  $2.0\,V$  and  $4.5\,V$ . The NiFe@NC/PPC cathode can deliver high

specific capacities of  $3\,\mathrm{mA}\,h$  cm $^{-2}$  with a columbic efficiency of 95%, even at a higher current density of  $0.1\,\mathrm{mA}\,\mathrm{cm}^{-2}$ . In addition, the discharge plateau is stable and maintained at  $2.64\,\mathrm{V}$ . The higher discharge capacity and columbic efficiency further demonstrate that NiFe@NC/PPC cathode possess excellent catalytic activity towards the electrochemical reactions of Li-CO<sub>2</sub> batteries. With the increase of current density, the capacity decreases to  $2.3\,\mathrm{mA}\,h$  cm $^{-2}$ ,  $0.95\,\mathrm{mAh}\,\mathrm{cm}^{-2}$  and  $0.3\,\mathrm{mA}\,h$  cm $^{-2}$  at current density values of  $0.2\,\mathrm{mA}\,\mathrm{cm}^{-2}$ ,  $0.5\,\mathrm{mA}\,\mathrm{cm}^{-2}$  and  $1\,\mathrm{mA}\,\mathrm{cm}^{-2}$ , respectively.

For the exploration of cycle stability, the NiFe@NC/PPC cathodes were measured at a current density of 0.05 mA cm $^{-2}$  with the cut-off capacity of 0.25 mAh cm $^{-2}$ . From Fig. 6c, it is clear that the NiFe@NC/PPC cathodes exhibit a relatively low charge plateau at 3.78 V in the first cycle. Moreover, the discharge plateau maintained at about 2.7 V even after 50 cycles, indicating the excellent catalytic ability for  $\rm CO_2$  reduction and decomposition ability of LiCO $_3$ . Interestingly, the discharge platform slightly increased and then reduce with the increase of

**Table 1**The performance of Li-CO<sub>2</sub> batteries with different cathodes.

Cathodes	Current density	Specific Capacity (mAh $g_{catalyst}^{-1}$ )	Specific Capacity (mAh $g_{cathode}^{-1}$ )	Cycle Stability	Refs
Cu/N-G	200 mA g <sup>-1</sup> (~0.06 mA)	14864	445.9	50	[9]
Ni/N-G	$100 \text{ mA g}^{-1} \ (\sim 0.03 \text{ mA})$	17652	529.5	101	[10]
	$200 \text{ mA g}^{-1} \ (\sim 0.06 \text{ mA})$	4000	120		
NiO-CNTs	$50 \text{ mA g}^{-1} \ (\sim 0.015 \text{ mA})$	9000	270	42	[36]
Ru/Super P	$100 \text{ mA g}^{-1} \ (\sim 0.05 \text{ mA})$	8229.5	411.5	70	[8]
B, N-G	$300 \text{ mA g}^{-1} \ (\sim 0.05 \text{ mA})$	14996	749.8	200	[16]
Mo <sub>2</sub> C/CNT	20 mA (~0.02 mA)	287.5	82.1	40	[35]
NiFe@NC/PPC	0.05 mA cm <sup>-2</sup> (~0.04 mA)		518	109	This work

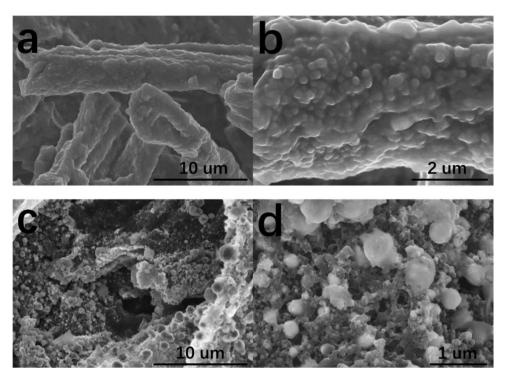


Fig. 7. SEM images of NiFe@NC/PPC cathodes after 1st discharge (a, b), and 1st charge (c, d).

cycling numbers. In the first few cycles, the discharge voltage gradually increased, which may be due to the gradual infiltration of electrolyte and electrode activation process. In the following cycles, the surface of the catalyst was covered by the uncompleted  $\rm Li_2CO_3$  in each cycle, resulting in the decrease of catalyst activity and discharge voltage. The comparison of the cyclic stability of NiFe@NC/PPC and NiFe@NC/CP is presented in Fig. 6d. It is clear that the NiFe@NC/CP could only maintain 13 cycles and the charge potential exceeded 4.5 V. Nevertheless, NiFe@NC/PPC cathodes not only could sustain 109 cycles, but also exhibit lower charge overpotential < 4.3 V even at the ending of cycle testing, which possess enhanced cycle stability in comparison to NiFe@NC/CP.

The reversible formation and decomposition of  $\rm Li_2CO_3$  were investigated by FE-SEM and XPS. As shown in Figs. 7a and 7b, it is clear that the insolubility  $\rm Li_2CO_3$  was deposited on the surface of electrode after discharge to 2.0 V, while the fibrous structure of NiFe@NC/PPC was retained.

After being charged to 4.5 V, almost all of the discharged products disappear and the surface of NiFe@NC/PPC afresh exposes the channels and microporous, as shown in Figs. 7c and 7d. This result indicates the high reversibility of the NiFe@NC/PPC cathode upon cycling. It is believed that the unique porous structure provides sufficient space for  $\text{Li}_2\text{CO}_3$  deposition and ensures uniform  $\text{CO}_2$  transport and electrolyte infiltration, while the excellent catalytic ability enhances the interactions between  $\text{Li}_2\text{CO}_3$  and NiFe@NC/PPC.

Fig. 8 show the XPS spectra of C 1 s of the NiFe@NC/PPC cathode after the 1st discharge/recharge (Figs. 8a and 8b) and after 100 cycles at limited capacity mode (Figs. 8c and 8d) at 0.05 mA cm $^{-2}$ . Clearly, a sharp peak at 289.8 eV can be observed after 1st discharge, which attributed to the discharge product of Li<sub>2</sub>CO<sub>3</sub> (Fig. 8a) [8].

However, the signal of  $\rm Li_2CO_3$  significantly reduced in the XPS spectra of the electrode after recharge (Fig. 8b), indicating that most of the  $\rm Li_2CO_3$  could be decomposed during the recharge process, which demonstrating the good reversibility performance of NiFe@NC/PPC cathode. Yang et al. [8] researched the charging process of  $\rm Li\text{-}CO_2$  battery. They believed that  $\rm Li_2CO_3$  would be decomposed only when the charge voltage higher than 4.7 V, without the application of

catalyst. At this potential, the electrolyte has been decomposed, and the possibility of battery cycling is zero. The catalyst can reduce the charge voltage and eliminate of superoxide radicals caused by self-decomposition of  $\text{Li}_2\text{CO}_3$ , thus ensuring the battery cycle. This theory also reflects the role of NiFe@NC/PPC, which can promote the occurrence of adverse reactions (Li + CO<sub>2</sub> $\rightleftarrows$ Li<sub>2</sub>CO<sub>3</sub> + C). To illustrate the reversibility of the battery, the XPS was conducted to investigate the discharge product at the limited capacity cycle mode.

As shown in Figs. 8c and 8d, the XPS peak of  $\rm Li_2CO_3$  maintained a certain intensity after 100th recharge compared with that of discharged cathode after  $100^{th}$  cycle. Therefore, we can infer that a small amount of  $\rm Li_2CO_3$  may be left after the end of each cycle. The accumulation of  $\rm Li_2CO_3$  results in passivation of electrode and blockage of transfer channel for  $\rm CO_2$  and electrolyte, which eventually leads to battery failure.

#### 4. Conclusions

In summary, the discarded biomass (pomelo peels) were used as raw materials and the NiFe-Prussian blue analogues deposited on it to form NiFe-PBA/PP precursor. Followed by carbonization at 1000 °C in Ar atmosphere, the finally obtained 3D free-standing NiFe@NC/PPC cathode was employed as the cathode for Li- $CO_2$  batteries. SEM images confirmed that this cathode inherits the 3D porous structure of biomassderived carbon materials, which offer sufficient space for the Li<sub>2</sub>O<sub>2</sub> deposition and facilitate mass transport. In addition, this cathode possess high catalytic activity towards CO2 reduction reaction and Li2CO3 decomposition reaction. Benefited from the unique 3D porous characteristics and the superior catalytic activity of the NiFe@NC/PPC composite, Li-CO2 batteries with NiFe@NC/PPC cathodes delivered high discharge capacity and excellent cyclic stability with stable discharge and charge platforms. XPS analysis revealed that a trace amount of Li<sub>2</sub>CO<sub>3</sub> cannot be decomposed in each cycle, which may accumulate on the surface of electrode and cover the catalytic active sites, leading to battery failure.

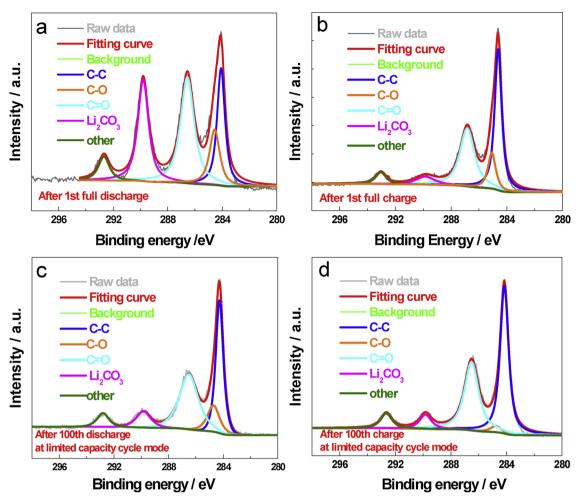


Fig. 8. XPS spectrum of NiFe@NC/PPC cathodes at different discharge/recharge stages.

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### Appendix A. Supplementary data

Supplementary material related to this article can be found, in the online version, at doi:https://doi.org/10.1016/j.apcatb.2018.11.075.

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